

In the claims:

Please amend the claims as shown below:

5 1. (Currently amended) A method for continuous alkali oxygen delignification of digested cellulose pulp and of cellulose pulp that has been washed after digestion, comprising:
~~which storing pulp is stored in a storage tower or pulp chute at essentially atmospheric pressure, and that~~
10 ~~maintaining~~ a medium consistency of the pulp in ~~at~~he range of 8-18%, ~~and that~~ maintaining the cellulose pulp to be delignified at a kappa value of at least 15 units, ~~or~~ preferably a kappa exceeding 20 units, where the oxygen delignification ~~taking~~ takes place in a reactor system with
15 several oxygen reactors with a predetermined retention time of the cellulose pulp in the reactor system, where ~~adding~~ alkali is added to the cellulose pulp in order to obtain an initial pH exceeding 9.0 and ~~adding~~ where oxygen is added to the cellulose pulp at an amount of 5-50 kg per tonne of pulp at a position before a first oxygen reactor in the reactor system, ~~providing~~ and where the pulp ~~with~~ has a predetermined total retention time of greater than 45 minutes in the reactor system, ~~characterised in that, in association with~~ the addition of the necessary chemicals ~~chemicals~~ and an initial mixing-in operation,
25 ~~placing~~ the cellulose pulp ~~is~~ placed under pressure at an initial pressure of greater than 15.0 bar, ~~subjecting~~ after which the pulp ~~is~~ subject to more than one remixing position where ~~at~~ the final pressure after ~~at~~ the final remixing position is at least 13 bar, ~~subjecting the pulp to~~ and with a minimum retention time ~~in a high~~ in this first high pressure section of at least 3-10 minutes,
30 ~~reducing~~ after which the pressure of the pulp ~~is~~ reduced to a pressure that lies under 10-12 bar, ~~heating the pulp with~~

and is heated by steam such that at the temperature of the pulp is raised by at least 5 °C by the addition of steam, and leading followed by the heated pulp being led to a reactor system in a low pressure section with a retention time that exceeds the retention time in the high pressure section.

2. (Currently amended) The method according to claim 1, ~~characterised in that~~ wherein oxygen, preferably the major part of the oxygen added for the oxygen stage, is added to the cellulose pulp immediately after the initial pressure of more than 15 bar has been established.
3. (Currently amended) The method according to claim 2, ~~characterised in that~~ wherein the remixing positions are constituted by fluidising mixers, either in at the form of a fluidising pump, a fluidising restriction, a fluidising mixer or a restriction in at the flow that results in a fall in pressure of less than 1 bar.
4. (Currently amended) The method according to claim 3, ~~characterised in that~~ wherein a first high pressure reactor is located after the initial mixing-in operation, in which reactor the cellulose pulp is given a first retention time of t_1 , and in that a high pressure reactor follows after the remixing positions in the high pressure section after each one of the remixing positions.
5. (Currently amended) The method according to claim 4, ~~characterised in that~~ wherein the reactors in the high pressure section are dimensioned such that the cellulose pulp is given successively longer retention times, such that when if the number of reactors is X , the retention times are $t_1 - t_x$ for each relevant reactor $R_1 - R_x$, where $t_1 < t_2 < \dots < t_x$.

6. (Currently amended) The method according to claim 5,
characterised in that wherein the retention times t_1
- t_x in the reactors R_1 - R_x in the high pressure section
5 are expressed as
 $t_{\min} = 1$ minute for t_1 , after which ($t_x=2 * t_{x-1}$) and $T_{\max}=$
 $X * 10$ minutes;
 $(t_1=1-10 \text{ min.}, t_2=2-20 \text{ min.}, t_3=4-30$
10 min.; $t_4=8-40$ min. etc.),
where $t_x < t_{x+1}$.

7. (Currently amended) The method according to any one of the
preceding claims, characterised in that claim 1
15 wherein a stirrer is present in at least one high pressure
reactor, which stirrer acts in at the principal part (greater
than 50%) of at the reactor volume, either in at the form of a
mechanical stirrer (S) or hydrodynamic stirrers that at
least circulate free fluid in the reactor.

20 8. (Currently amended) The method according to any one of the
preceding claims, characterised in that claim 1
wherein at least one of the oxygen and and alkali additions
25 are can be added to the cellulose pulp in association with
the remixing positions in the high pressure section at an
amount that is lower than the amount that is added at the
initial mixing-in operation, and in that at least one of
the oxygen and alkali additions are can be added batch-wise
at at the beginning of the low pressure section.

30 9. (Currently amended) The method according to any one of the
preceding claims, characterised in that claim 1
wherein the cellulose pulp is dewatered before the oxygen
delignification to a higher consistency and in that it the
35 cellulose pulp is re-diluted before the oxygen
delignification to a medium consistency with pure filtrate

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that has preferably been previously oxidized, and in that alkali in at the form of oxidized white liquor is used in the oxygen delignification.